## Fluid \& Gas Properties

## FLUID DENSITY

Density is the ratio of mass to volume. In English, units density is expressed in pounds mass/cubic foot $\left(\mathrm{lbm} / \mathrm{ft}^{3}\right)$. The symbol for density is $\rho$. Density is usually written as:

$$
\rho=\mathrm{lbm} / \mathrm{ft}^{3}
$$

The density for a liquid is normally taken from a table. Table 1 lists the densities of various liquids. For steam, the density is typically read from the steam tables for the desired pressure and temperature. For a gas, density is usually calculated using the ideal gas law. The ideal gas law is:

$$
\rho=\mathrm{p} / \mathrm{RT}
$$

where $\mathrm{p}=$ pressure
$\mathrm{R}=$ gas constant
$\mathrm{T}=$ temperature

## SPECIFIC VOLUME

Specific volume is the reciprocal of density and is the volume occupied by 1 lbm of fluid.

$$
v=1 / \rho
$$

Table 2 gives the specific volume for saturated steam at various temperatures and pressures.

## SPECIFIC GRAVITY

Specific gravity is the ratio of a fluid's density to some reference density. For liquids, the reference density is the density of pure water. Strictly speaking, specific gravity of a liquid cannot be given without specifying the reference temperature at which the water's density was evaluated. The density of water in English units is normally referenced at $32^{\circ} \mathrm{F}$ and is $62.43 \mathrm{lbm} / \mathrm{ft}^{3}$. Using this as the reference density, specific gravity is given as:

$$
\text { S.G. }=\frac{\text { density }}{62.431 \mathrm{bm} / \mathrm{ft}^{3}}
$$

## RELATIVE DENSITY

Relative density is the ratio of the density of one substance to that of another, both at the same temperature. The use of specific gravity to describe this quantity is discouraged, partially due to the fact there is no stipulation that the temperatures be equal in specific gravity measurements.
For gasses, the relative density is generally the ratio of the density of the gas to that of air, again both at the same temperature, and also at the same pressure and dryness.

Relative densities of petroleum products and aqueous acid solutions can be found using a device called a hydrometer. In addition to the hydrometer scale that references water, there are two basic hydrometer scales, the Baume scale and the API (American Petroleum Industry Scale). The Baume scale was widely used in the past but the API scale is now recommended for use with all liquids.
The API scale can be used with all liquids:

$$
\text { Relative Density }=\frac{141.5}{131.5+^{\circ} \mathrm{API}}
$$

Table 3 lists the relative densities corresponding to the API scale.
For liquids lighter than water, their specific gravity can be found from the Baume hydrometer reading using this equation:

$$
\text { Relative Density }=\frac{140.0}{130.0+{ }^{\circ} \text { Baume }}
$$

For liquids heavier than water, their specific gravity can be found from the Baume hydrometer reading using this equation:

$$
\text { Relative Density }=\frac{145.0}{145.0-^{\circ} \text { Baume }}
$$

Relative densities can also be given for gases. The reference density is that of air at specified temperature and pressure. Since both the gas and air are evaluated at the same pressure and temperature, the relative density is the inverse of the ratio of the gas constants.

TABLE 1 Density of Liquids

| Liquid | Temperature ${ }^{\circ}$ F | Density lbm/ft ${ }^{3}$ | Specific Gravity redl $\mathrm{H}_{2} \mathrm{O} @ 60^{\circ} \mathrm{F}$ |
| :---: | :---: | :---: | :---: |
| Acetaldehyde | 64 | 48.9 | 0.784 |
| Acetone | 60 | 49.4 | 0.792 |
| Acetic Anhydride | 68 | 67.5 | 1.083 |
| Acetic Acid (conc) | 68 | 65.5 | 1.050 |
| Ammonia | 10 | 40.9 | 0.656 |
| Aniline | 68 | 63.8 | 1.023 |
| Benzene | 32 | 56.1 | 0.899 |
| Benzoic Acid | 59 | 79.0 | 1.267 |
| Brine, 10\% CaCl | 32 | 68.1 | 1.091 |
| Brine, 10\% NaCl | 32 | 67.2 | 1.078 |
| Butyric Acid (conc) | 68 | 60.2 | 0.965 |
| Carbon Disulfide | 32 | 80.6 | 1.292 |
| Carbon Tetrachloride | 68 | 99.6 | 1.597 |
| Chlorobenzene | 68 | 69.1 | 1.108 |
| Chloroform | 68 | 92.9 | 1.489 |
| Cresol, Meta | 68 | 64.5 | 1.035 |
| Diphenyl | 163 | 61.9 | 0.993 |
| Distillate | 60 | 53.0 | 0.850 |
| Fuel Oil \#6 (min) | 60 | 61.9 | 0.993 |
| Furfural | 68 | 72.3 | 1.160 |
| Gasoline | 60 | 46.8 | 0.751 |
| Gasoline (natural) | 60 | 42.4 | 0.680 |
| Glycerin | 112 | 78.6 | 1.261 |
| Heptane | 68 | 42.7 | 0.685 |
| Hydrochloric Acid (42.5\%) | 64 | 92.3 | 1.400 |
| Hydrocyanic Acid | 64 | 43.5 | 0.697 |
| Kerosene | 60 | 50.8 | 0.815 |
| Mercury | 20 | 849.7 | 13.623 |
|  | 40 | 848.0 | 13.596 |
|  | 60 | 846.3 | 13.568 |
|  | 80 | 844.6 | 13.541 |
|  | 100 | 842.9 | 13.514 |
| Methylene Chloride | 68 | 83.4 | 1.337 |
| Milk | -- | 64.2-64.6 | -- |
| Nitric Acid (conc) | 64 | 93.7 | 1.502 |
| Olive Oil | 59 | 57.3 | 0.919 |
| Ortho-phosphoric Acid | 65 | 114.4 | 1.834 |
| Pentane | 59 | 38.9 | 0.624 |
| Phenol | 77 | 66.8 | 1.072 |
| Toluene | 68 | 54.1 | 0.867 |
| Xylene | 68 | 55.0 | 0.882 |

TABLE 2 Properties of Saturated Steam

| Pressure PSIA | $\underset{\substack{\text { Temp } \\{ }^{\circ} \mathbf{F}}}{ }$ | Sp. Vol. $\mathrm{ft}^{3} / \mathrm{lbm}$ | Pressure PSIA | $\underset{\substack{{ }^{\circ} \mathbf{F} \\ \hline}}{ }$ | Sp. Vol. <br> $\mathbf{f t}^{3} / \mathrm{lbm}$ | Pressure PSIA | $\begin{array}{\|c} \hline \text { Temp } \\ { }^{\circ} \mathbf{F} \end{array}$ | Sp. Vol. $\mathrm{ft}^{3} / \mathrm{lbm}$ |
| :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 0.50 | 79.58 | 641.4 | 80.0 | 312.03 | 5.472 | 250.0 | 400.95 | 1.8438 |
| 1.0 | 101.74 | 333.6 | 85.0 | 316.25 | 5.168 | 275.0 | 409.43 | 1.6804 |
| 2.0 | 126.08 | 173.73 | 90.0 | 320.27 | 4.896 | 300.0 | 417.33 | 1.5433 |
| 3.0 | 141.48 | 118.71 | 95.0 | 324.12 | 4.652 | 350.0 | 431.72 | 1.3260 |
| 4.0 | 152.97 | 90.63 | 100.0 | 327.81 | 4.432 | 400.0 | 444.59 | 1.1613 |
| 5.0 | 162.24 | 73.52 | 105.0 | 331.36 | 4.232 | 450.0 | 456.28 | 1.0320 |
| 10.0 | 193.21 | 38.42 | 110.0 | 334.77 | 4.049 | 500.0 | 467.01 | 0.9278 |
| 14.7 | 212.00 | 26.80 | 115.0 | 338.07 | 3.882 | 550.0 | 476.93 | 0.8422 |
| 15.0 | 213.03 | 26.29 | 120.0 | 341.25 | 3.728 | 600.0 | 486.21 | 0.7698 |
| 20.0 | 227.96 | 20.089 | 125.0 | 344.33 | 3.587 | 650.0 | 494.90 | 0.7085 |
| 25.0 | 240.07 | 16.303 | 130.0 | 345.32 | 3.455 | 700.0 | 503.10 | 0.6554 |
| 30.0 | 250.33 | 13.746 | 135.0 | 350.21 | 3.333 | 750.0 | 510.85 | 0.6094 |
| 35.0 | 259.28 | 11.898 | 140.0 | 353.02 | 3.220 | 800.0 | 518.23 | 0.5687 |
| 40.0 | 267.25 | 10.498 | 145.0 | 355.76 | 3.114 | 850.0 | 525.26 | 0.5328 |
| 45.0 | 274.44 | 9.401 | 150.0 | 358.42 | 3.015 | 900.0 | 531.98 | 0.5006 |
| 50.0 | 281.01 | 8.515 | 160.0 | 363.53 | 2.834 | 950.0 | 538.42 | 0.4718 |
| 55.0 | 287.07 | 7.787 | 170.0 | 368.41 | 2.675 | 1000 | 544.61 | 0.4456 |
| 60.0 | 292.71 | 7.175 | 180.0 | 373.06 | 2.532 | 1250 | 572.42 | 0.3450 |
| 65.0 | 297.97 | 6.665 | 190.0 | 377.51 | 2.404 | 1500 | 596.23 | 0.2765 |
| 70.0 | 302.92 | 6.206 | 200.0 | 381.79 | 2.288 | 1750 | 617.09 | 0.2267 |
| 75.0 | 307.60 | 5.816 | 225.0 | 391.79 | 2.042 | 2000 | 635.82 | 0.1878 |

TABLE 3 Relative Density at $\mathbf{6 0} / 60^{\circ} \mathrm{F}$ Corresponding to the API Scale

| Degree <br> API | Relative <br> Density | Pound <br> US Gal. | Degree <br> API | Relative <br> Density | Pound <br> US Gal. | Degree <br> API | Relative <br> Density | Pound <br> US Gal. |
| :--- | :---: | :---: | :---: | :---: | :---: | :---: | :---: | :---: |
| 10 | 1.0000 | 8.328 | 41 | 0.8203 | 6.830 | 71 | 0.6988 | 5.817 |
| 11 | 0.9930 | 8.270 | 42 | 0.8155 | 6.790 | 72 | 0.6953 | 5.788 |
| 12 | 0.9861 | 8.212 | 43 | 0.8109 | 6.752 | 73 | 0.6919 | 5.759 |
| 13 | 0.9792 | 8.155 | 44 | 0.8063 | 6.713 | 74 | 0.6886 | 5.731 |
| 14 | 0.9725 | 8.099 | 45 | 0.8017 | 6.675 | 75 | 0.6852 | 5.703 |
| 15 | 0.9659 | 8.044 | 46 | 0.7972 | 6.637 | 76 | 0.6819 | 5.676 |
| 16 | 0.9593 | 7.989 | 47 | 0.7927 | 6.600 | 77 | 0.6787 | 5.649 |
| 17 | 0.9529 | 7.935 | 48 | 0.7883 | 6.563 | 78 | 0.6754 | 5.622 |
| 18 | 0.9465 | 7.882 | 49 | 0.7839 | 6.526 | 79 | 0.6722 | 5.595 |
| 19 | 0.9402 | 7.830 | 50 | 0.7796 | 6.490 | 80 | 0.6690 | 5.568 |
| 20 | 0.9340 | 7.778 | 51 | 0.7753 | 6.455 | 81 | 0.6659 | 5.542 |
| 21 | 0.9279 | 7.727 | 52 | 0.7711 | 6.420 | 82 | 0.6628 | 5.516 |
| 22 | 0.9218 | 7.676 | 53 | 0.7669 | 6.385 | 83 | 0.6597 | 5.491 |
| 23 | 0.9159 | 7.627 | 54 | 0.7628 | 6.350 | 84 | 0.6566 | 5.465 |
| 24 | 0.9100 | 7.578 | 55 | 0.7587 | 6.316 | 85 | 0.6537 | 5.440 |
| 25 | 0.9042 | 7.529 | 56 | 0.7547 | 6.283 | 86 | 0.6506 | 5.415 |
| 26 | 0.8984 | 7.481 | 57 | 0.7507 | 6.249 | 87 | 0.6476 | 5.390 |
| 27 | 0.8927 | 7.434 | 58 | 0.7467 | 6.216 | 88 | 0.6446 | 5.365 |
| 28 | 0.8871 | 7.387 | 59 | 0.7428 | 6.184 | 89 | 0.6417 | 5.341 |
| 29 | 0.8816 | 7.341 | 60 | 0.7389 | 6.151 | 90 | 0.6388 | 5.316 |
| 30 | 0.8762 | 7.296 | 61 | 0.7351 | 6.119 | 91 | 0.6360 | 5.293 |
| 31 | 0.8708 | 7.251 | 62 | 0.7313 | 6.087 | 92 | 0.6331 | 5.269 |
| 32 | 0.8654 | 7.206 | 63 | 0.7275 | 6.056 | 93 | 0.6303 | 5.246 |
| 33 | 0.8602 | 7.163 | 64 | 0.7238 | 6.025 | 94 | 0.6275 | 5.222 |
| 34 | 0.8550 | 7.119 | 65 | 0.7201 | 5.994 | 95 | 0.6247 | 5.199 |
| 35 | 0.8498 | 7.076 | 66 | 0.7165 | 5.964 | 96 | 0.6220 | 5.176 |
| 36 | 0.8448 | 7.034 | 67 | 0.7128 | 5.934 | 97 | 0.6193 | 5.154 |
| 37 | 0.8398 | 6.993 | 68 | 0.7093 | 5.904 | 98 | 0.6160 | 5.131 |
| 38 | 0.8348 | 6.951 | 69 | 0.7057 | 5.874 | 99 | 0.6139 | 5.109 |
| 39 | 0.8299 | 6.910 | 70 | 0.7022 | 5.845 | 100 | 0.6112 | 5.086 |
| 40 | 0.8251 | 0.870 |  |  |  |  |  |  |

## ACFM vs. SCFM

It is often desirable to express a gas flow in terms of a "standard" volumetric flowrate. One of the most common forms encountered is standard cubic feet per minute (scfm). To convert an actual flowrate reading, here referred to as actual cubic feet per minute (acfm), it is necessary to multiply the actual flowrate by the ratio of the standard condition's specific volume over the actual condition's specific volume.

$$
\begin{aligned}
& \mathrm{Q}_{\mathrm{S}}=\mathrm{Q}_{\mathrm{A}}\left[v_{\mathrm{S}} / v_{\mathrm{A}}\right] \\
\text { where: } & \mathrm{Q}_{\mathrm{S}}=\text { flowrate in } \mathrm{scfm} \\
& \mathrm{Q}_{\mathrm{A}}=\text { flowrate in acfm } \\
& v_{\mathrm{S}}=\text { standard conditions specific volume } \\
& v_{\mathrm{A}}=\text { actual conditions specific volume }
\end{aligned}
$$

The ratio $v_{S} / v_{\mathrm{A}}$ can be written as:

$$
\left[\mathrm{T}_{\mathrm{S}} \mathrm{P}_{\mathrm{A}} / \mathrm{P}_{\mathrm{S}} \mathrm{~T}_{\mathrm{A}}\right]
$$

## IDEAL GAS BEHAVIOR

A gas can be considered ideal if it exhibits ideal gas behavior. Typically, gases at low pressures and at temperatures much higher than their critical temperatures can be treated as ideal gases. When the volume occupied by the gas molecules is negligible in comparison to the total volume, it is acceptable to treat the gas as an ideal gas. The benefit of treating gases as ideal is that it greatly simplifies the math required to evaluate their behavior.
There are two basic laws that define the behavior of ideal gases; they are Boyle's and Charle's Law. Boyle's law states that the volume and pressure of an ideal gas vary inversely when the temperature is held constant and is written as:

$$
\mathrm{p}_{1} \mathrm{~V}_{1}=\mathrm{p}_{2} \mathrm{~V}_{2}
$$

The second law is Charle's law that states when pressure is held constant, volume and temperature vary proportionally. Charle's law is written:

$$
\frac{\mathrm{T}_{1}=\mathrm{T}_{2}}{\mathrm{~V}_{1} \mathrm{~T}_{2}}
$$

The ideal gas law relates the pressure, temperature, and volume to the amount of gas present. The ideal gas law states that equal volumes of different gases at the same temperature and pressure contain the same number of molecules. The ideal gas law is written:

$$
\mathrm{pV}=\mathrm{nR} * \mathrm{~T}
$$

R* is known as the universal gas constant. It is universal because the same number can be used with any gas. Due to the different units that can be used for pressure, temperature, and volume, there are different values of $\mathrm{R}^{*}$. Table 4 lists values for $\mathrm{R}^{*}$.

The ideal gas law can be used with more than 1 mole of gas. If there are $n$ moles, the equation is written as:

$$
\mathrm{n}=\mathrm{m} / \mathrm{M}
$$

TABLE 4 Values of Universal Gas Constant

| 1545.33 | ft-lbf/pmole- ${ }^{\circ} \mathrm{R}$ |
| :---: | :---: |
| 0.08206 | atm-liter/gmole- ${ }^{\circ} \mathrm{K}$ |
| 1.986 | BTU/pmole- ${ }^{\circ} \mathrm{R}$ |
| 1.986 | cal/gmole- ${ }^{\circ} \mathrm{K}$ |
| 8.314 | joule/gmole- ${ }^{\circ} \mathrm{K}$ |
| 0.730 | atm-ft3/pmole- ${ }^{\circ} \mathrm{R}$ |

The ideal gas law can be rewritten taking into account the molecular weight of the specific gas. The specific gas constant is unique for each gas.

$$
\begin{aligned}
& \mathrm{pV}=\mathrm{mR} * \mathrm{t} / \mathrm{M} \\
& \mathrm{pV}=\mathrm{mT}(\mathrm{R} * / \mathrm{M}) \\
& \mathrm{pV}=\mathrm{mRT}
\end{aligned}
$$

Table 5 lists the properties of common gases.
Since density is the reciprocal of specific volume, the ideal gas law can be used to determine the density of an ideal gas. If $\mathrm{m}=1$, then the ideal gas law can be rewritten as:

$$
\begin{aligned}
& \mathrm{p}=\frac{1 \mathrm{RT}}{v} \\
& \mathrm{p}=\mathrm{RT} \\
& \rho=\frac{\mathrm{p}}{\mathrm{RT}}
\end{aligned}
$$

## PROPERTIES OF REAL GASES

Unfortunately, it is not always possible to achieve acceptable results by using the ideal gas law. It is very common for gases at low temperatures and/or high pressures to exhibit real gas behavior.
When the spacing between the gas molecules is small, they tend to attract each other. These attractive forces are called Van der Waals forces. Van der Waal's equation of state can be used to describe the behavior of real gases. Van der Waal's equation of state is written as:

$$
\frac{(\mathrm{p}+\mathrm{a})(\mathrm{V}-\mathrm{b})}{\mathrm{V}^{2}}=\mathrm{nR} * \mathrm{~T}
$$

For an ideal gas, $a$ and $b$ are zero and Van der Waal's equation reduces to the familiar ideal gas law.
Since real gas molecules tend to attract each other, the actual pressure exerted by a real gas is less than that predicted by the ideal gas law. The reduction in pressure is corrected for in the Van der Waal equation by the term ( $\mathrm{a} / \mathrm{V} 2$ ). The constant b is dependent on the volume occupied by the gas molecules in the dense state. Table 6 gives the values for $a$ and $b$ of common gases. The Van der Waal equation is typically used only when the gas is below critical pressure.

TABLE 5 Properties of Common Gases

| Gas | Symbol | MW | R | Density | k |
| :--- | :--- | :--- | :--- | :--- | :--- |
| Acetylene | $\mathrm{C}_{2} \mathrm{H}_{2}$ | 26.0 | 59.4 | 0.07323 | 1.30 |
| Air | -- | 29.0 | 53.3 | 0.08071 | 1.40 |
| Ammonia | $\mathrm{NH}_{3}$ | 17.0 | 91.0 | 0.04813 | 1.32 |
| Argon | A | 39.9 | 38.7 | 0.11135 | 1.67 |
| Carbon Dioxide | $\mathrm{CO}_{2}$ | 44.0 | 35.1 | 0.12341 | 1.28 |
| Carbon Monoxide | $\mathrm{CO}_{2}$ | 28.0 | 55.2 | 0.07806 | 1.40 |
| Chlorine | $\mathrm{Cl}_{2}$ | 70.9 | 21.8 | 0.2006 | 1.33 |
| Ethane | $\mathrm{C}_{2} \mathrm{H}_{6}$ | 30.07 | 51.3 | 0.08469 | 1.18 |
| Ethylene | $\mathrm{C}_{2} \mathrm{H}_{4}$ | 28.0 | 55.1 | 0.07868 | 1.22 |
| Freon (R-12) | $\mathrm{CCl}_{2} \mathrm{~F}_{2}$ | 120.9 | 12.6 | --- | 1.13 |
| Helium | $\mathrm{He}_{2}$ | 4.0 | 386.3 | 0.01114 | 1.66 |
| Hydrogen | $\mathrm{H}_{2}$ | 2.0 | 766.8 | 0.00561 | 1.41 |
| Isobutane | $\mathrm{C}_{4} \mathrm{H}_{10}$ | 58.12 | 26.6 | --- | 1.09 |
| Krypton | $\mathrm{Kr}_{2}$ | 82.9 | 18.6 | 0.2315 | 1.67 |
| Methane | $\mathrm{CH}_{4}$ | 16.0 | 96.4 | 0.04475 | 1.32 |
| Neon | $\mathrm{Ne}_{2}$ | 20.18 | 76.4 | 0.05621 | 1.64 |
| Nitrogen | $\mathrm{N}_{2}$ | 28.0 | 55.2 | 0.07807 | 1.40 |
| Oxygen | $\mathrm{O}_{2}$ | 32.0 | 48.3 | 0.08921 | 1.40 |
| Propane | $\mathrm{C}_{3} \mathrm{H}_{8}$ | 44.09 | 35.0 | 0.1254 | 1.12 |
| Steam** | $\mathrm{H}_{2} \mathrm{O}$ | 18.0 | 85.8 | --- | 1.28 |
| Sulfur Dioxide | $\mathrm{SO}_{2}$ | 64.1 | 24.0 | 0.1827 | 1.26 |
| Xenon | $\mathrm{Xe}^{2}$ | 130.2 | 11.9 | --- | 1.67 |

** Values for steam are approximate and may be used only for low pressures and high temperatures. $R$ is in ft-lbf/lbm- ${ }^{\circ}$, Density is in lbm/ft ${ }^{3}$ at $32^{\circ} \mathrm{F}$ and 14.7 PSIA.

TABLE 6 Values of $\mathbf{a}$ and $\mathbf{b}$ for Common Gases

|  | a(atm-ft $\left.{ }^{6} / \mathbf{\text { pmole }}\right)$ | $\mathbf{b}\left(\mathbf{f t}^{3} / \mathbf{\text { pmole }}\right)$ |
| :--- | :--- | :--- |
| Air | 345.2 | 0.585 |
| $\mathrm{CO}_{2}$ | 926 | 0.686 |
| $\mathrm{H}_{2}$ | 62.8 | 0.427 |
| $\mathrm{O}_{2}$ | 348 | 0.506 |
| Steam | 1400 | 0.488 |

There is another correction factor that is applied to real gases. This factor is known as the compressibility factor, and is sometimes used for correction of gas flows through orifices. The compressibility factor is denoted by Z , and is dependent on pressure, temperature, and the type of gas. The modified ideal gas law is:

$$
\mathrm{pV}=\mathrm{ZRT}
$$

Correction factors for gases can be plotted against pressure and temperature. By using the principle of corresponding states, it is possible to create one graph that covers multiple gases. The principle of corresponding states says that all gases behave alike whenever they have the same reduced variables. The reduced variables that the law refers to are the ratios of pressure, temperature, and volume to their critical values. Table 7 gives critical properties for selected gases.

$$
\begin{aligned}
& \mathrm{P}_{\mathrm{r}}=\mathrm{P} / \mathrm{P}_{\mathrm{c}} \\
& \mathrm{~T}_{\mathrm{r}}=\mathrm{T} / \mathrm{T}_{\mathrm{c}} \\
& \mathrm{~V}_{\mathrm{r}}=\mathrm{v} / \mathrm{V}_{\mathrm{c}}
\end{aligned}
$$

TABLE 7 Approximate Critical Properties

| gas | $\left.\mathbf{T}_{\mathbf{c}}{ }^{( }{ }^{\circ} \mathbf{R}\right)$ | $\mathbf{P}_{\mathbf{C}}(\mathbf{p s i a})$ |
| :--- | :--- | :--- |
| Air | 235.8 | 547.0 |
| Ammonia | 730.1 | 1639.0 |
| Argon | 272.2 | 705.0 |
| Carbon Dioxide | 547.8 | 1071.0 |
| Carbon Monoxide | 242.2 | 508.2 |
| Chlorine | 751.0 | 1116.0 |
| Ethane | 549.8 | 717.0 |
| Ethylene | 509.5 | 745.0 |
| Helium | 10.0 | 33.8 |
| Hydrogen | 60.5 | 188.0 |
| Mercury | 2109.0 | 2646.0 |
| Methane | 343.9 | 673.3 |
| Neon | 79.0 | 377.8 |
| Nitrogen | 227.2 | 492.5 |
| Oxygen | 278.1 | 730.9 |
| Propane | 666.3 | 617.0 |
| Sulfur Dioxide | 775.0 | 1141.0 |
| Water Vapor | 1165.4 | 3206.0 |
| Xenon | 521.9 | 855.3 |

Figures 1 and 2 are graphs of compressibility factors.


FIGURE 1 Compressibility Factors for Low Pressure as presented by Professor E. Obert and L.
Nelson in "Generalized P-V-T Properties of Gases," ASME Transactiona, 76, 1057 (1954)


FIGURE 2 Compressibility Factors for High Pressure

## VISCOSITY

The viscosity of a liquid is a measure of its resistance to flow. Liquids can be categorized by their viscosity properties. One of the most common liquid categories is Newtonian liquids.

Viscosity is measured using two parallel plates and a layer of fluid. The plates are separated from each other by a layer of fluid with a thickness of y. One plate is fixed and the other one is maintained at a constant velocity by a constant force $F$.

It has been shown that for Newtonian fluids, the force required to maintain the velocity is proportional to the velocity and inversely proportional to the separation of the plates.

$$
\frac{F}{A}=\frac{d v}{d y}
$$

The constant of proportionality is the absolute viscosity. The quantity F/A is the shear stress in the fluid. The equation can be written as:

$$
t=u(\mathrm{dv} / \mathrm{dy}) \rho
$$

Kinematic viscosity is also used commonly and is a combination of absolute viscosity and the density of the fluid.

$$
v=u \mathrm{~g} / \rho
$$

Tables 8 and 9 give conversion factors for the most commonly encountered viscosity units.

TABLE 8 Equivalents of Absolute Viscosity

| Absolute <br> Viscosity | Centipoise | Poise | Pound <br> Ft Sec |
| :--- | :---: | :---: | :---: |
| Centipoise | 1 | 0.01 | 0.000672 |
| Poise | 100 | 1 | 0.0672 |
| Pound | 1487 | 14.87 | 1 |
| Ft Sec |  |  |  |

TABLE 9 Equivalents of Kinematic Viscosity

| Kinematic <br> Viscosity | Centistoke | Stoke | $\underline{\mathbf{F t}^{2}}$ <br> Sec |
| :--- | :---: | :---: | :---: |
| Centistoke | 1 | 0.01 | 0.00001076 |
| Stoke | 100 | 1 | 0.001076 |
| $\mathrm{Ft}^{2}$ | 92,900 | 929 | 1 |
| Sec |  |  |  |

Table 10 lists the viscosity of common liquids and Table 11 lists the viscosity of common gases.

TABLE 10 Viscosity of Common Liquids

| Temperature ${ }^{\circ} \mathrm{F}$ | Viscosity Centipoise | Temperature ${ }^{\circ} \mathrm{F}$ | Viscosity Centipoise | Temperature ${ }^{\circ} \mathrm{F}$ | Viscosity Centipoise |
| :---: | :---: | :---: | :---: | :---: | :---: |
| Acetic Acid |  | Ethylene Oxide |  | Isohexane |  |
| 59 | 1.31 | -57 | 0.577 | 32 | 0.376 |
| 64 | 1.30 | -37 | 0.488 | 68 | 0.306 |
| 77 | 1.155 | -5.8 | 0.394 | 104 | 0.254 |
| 86 | 1.04 | 32 | 0.320 | Isopentane |  |
| 106 | 1.00 | Fluorbenzene |  | 32 | 0.273 |
| 212 | 0.43 | 68 | 0.598 | 68 | 0.223 |
| Acetic Anhydride |  | 140 | 0.389 | Kerosene |  |
| 32 | 1.24 | 212 | 0.275 | 68 | 2.69 |
| 59 | 0.971 | Fuel Oil, \#2 |  | 100 | 2.0 |
| 64 | 0.90 | 70 | 3.0-7.4 | Methyl Alcohol |  |
| 86 | 0.783 | 100 | 2.11-4.28 | -48 | 1.98 |
| 212 | 0.490 | Fuel Oil, \#6 |  | 32 | 0.82 |
| Acetone |  | 122 | 97.4-660 | 59 | 0.623 |
| 14 | 0.450 | 160 | 37.5-172 | 68 | 0.597 |
| 32 | 0.399 | Gasoline |  | 77 | 0.546 |
| 59 | 0.337 | 60 | 0.46-0.88 | 86 | 0.510 |
| 77 | 0.316 | 100 | 0.40-0.71 | Methyl Chloride |  |
| Ammonia |  | Glycerin |  | 0 | 0.25 |
| -92 | 0.475 | 32 | 12,110 | 20 | 0.23 |
| -58 | 0.317 | 43 | 6,260 | 40 | 0.21 |
| -40 | 0.276 | 59 | 2,330 | 60 | 0.19 |
| -28 | 0.255 | 68 | 1,490 | 100 | 0.16 |
| Benzene |  | 77 | 954 | Naphthalene |  |
| 32 | 0.912 | 86 | 629 | 176 | 0.967 |
| 50 | 0.758 | Heptane |  | 212 | 0.776 |
| 68 | 0.652 | 32 | 0.524 | Nitric Acid |  |
| 86 | 0.564 | 63 | 0.461 | 32 | 2.275 |
| 104 | 0.503 | 68 | 0.409 | Nitrobenzene |  |
| 122 | 0.542 | 77 | 0.386 | 37 | 2.91 |
| Carbon Tetrachloride |  | 104 | 0.341 | 42 | 2.71 |
| 32 | 1.329 | Hexane |  | 50 | 2.48 |
| 59 | 1.038 | 32 | 0.401 | 68 | 2.03 |
| 68 | 0.969 | 68 | 0.326 | Nitromethane |  |
| 86 | 0.843 | 77 | 0.386 | 32 | 0.853 |
| 104 | 0.739 | 104 | $0.341$ | 77 | 0.620 |
| 140 | 0.585 | Hyrdochloric Acid, 31.5\% |  | $\mathrm{n}-\mathrm{Oc}$ |  |
| Chlorine Liquid |  | 0 | 3.4 | 32 | 0.706 |
| -40 | 0.505 | 20 | 2.9 | 68 | 0.240 |
| -20 | 0.462 | 40 | 2.5 | 104 | 0.433 |
| 20 | 0.400 | 60 | 2.0 | Pentane |  |
| 60 | 0.350 | 80 | 1.8 | 32 | 0.289 |
| 100 | 0.313 | 100 | 1.6 | 68 | 0.524 |
| Ethylbenzene |  | 140 | 1.2 | ${ }_{65}$ Phenol 12.7 |  |
| 63 | 0.691 | Iodine Liquid |  | 65 | 12.7 |
| Ethylene Glycol |  | 241 | 2.27 | 122 | 3.49 |
| 68 | 19.9 | Isoheptane |  | 158 | 2.03 |
| 104 | 9.13 | 32 | 0.481 | 194 | 1.26 |
| 140 | 4.95 | 68 | 0.384 |  |  |
| 176 | 3.02 | 104 | 0.315 |  |  |

(continued)

TABLE 10 Viscosity of Common Liquids (continued)

| $\underset{{ }^{\circ} \mathrm{F}}{\substack{\text { Temperature }}}$ | Viscosity Centipoise | $\underset{{ }^{\circ} \mathrm{F}}{\substack{\text { Temperature }}}$ | Viscosity Centipoise | $\underset{{ }^{\circ} \mathrm{F}}{\substack{\text { Temperature }}}$ | Viscosity Centipoise |
| :---: | :---: | :---: | :---: | :---: | :---: |
| Phosphorus Liquid |  | Sodium Liquid |  | Sulfuric Acid |  |
| 71 | 2.34 | 0 | 2.4 | 32 | 48.4 |
| 88 | 2.01 | 26 | 1.3 | 59 | 32.8 |
| 110 | 1.73 | 40 | 1.2 | 68 | 25.4 |
| 123 | 1.60 | 60 | 1.1 | 86 | 15.7 |
| 140 | 1.45 | 100 | 1.0 | 104 | 11.5 |
| Sodium Hydroxide |  | 140 | 0.85 | 122 | 8.82 |
|  |  |  |  |  | 8.82 7.22 |
| 70 | 100 |  |  | Turpentine |  |
| 100 | 40 | 276 | 8.7 |  |  |
| 140 | 15 | 301 | 7.1 | 100 | 2.0 |
| 160 | 9.5 | 314 | 7.2 | Water |  |
| 200 | 3.7 | 317 | 7.6 | 60 | 1.13 |
| 220 | 2.4 | 319 | 14.5 | 130 | 0.55 |
| 250 | 1.4 | Sulfur Dioxide |  |  |  |
|  |  | -28 | 0.5508 |  |  |
|  |  | 13 | 0.4285 |  |  |
|  |  | 32 | 0.3936 |  |  |

TABLE 11 Viscosity of Common Gases

| Temperature ${ }^{\circ} \mathrm{F}$ | Viscosity Centipoise | Temperature ${ }^{\circ} \mathrm{F}$ | Viscosity Centipoise | $\underset{{ }^{\circ} \mathrm{F}}{\text { Temperature }}$ | Viscosity Centipoise |
| :---: | :---: | :---: | :---: | :---: | :---: |
| Acetylene |  | Carbon Monoxide |  | Nitrogen |  |
| 32 | 0.00935 | 32 | 0.0166 | -6.7 | 0.0156 |
| Air |  | 59 | 0.0172 | 51.6 | 0.0171 |
| 32 | 0.0171 | 260.8 | 0.0218 | 81 | 0.0178 |
| 104 | 0.0190 | Chlorine |  | 261 | 0.0219 |
| 444 | 0.0264 | 122 | 0.0147 | 440 | 0.0256 |
| 633 | 0.0305 | 212 | 0.0168 | Oxygen |  |
| 674 | 0.0312 | 302 | 0.0187 | 32 | 0.0189 |
| 768 | 0.0341 | 392 | 0.0208 | 67 | 0.0202 |
| Ammonia |  | Ethane |  | 262 | 0.0257 |
| 32 | 0.0092 | 32 | 0.0085 | 440 | 0.0302 |
| 68 | 0.0098 | 63 | 0.0090 | n-Pentane |  |
| 212 | 0.0128 | Ethylene |  | 77 | 0.0068 |
| 302 | 0.0146 | 32 | 0.0091 | 212 | 0.0084 |
| 482 | 0.0181 | 68 | 0.0101 | Propane |  |
| Argon |  | 122 | 0.0110 | 64.2 | 0.0079 |
| 32 | 0.0210 | 212 | 0.0126 | 213 | 0.0101 |
| 68 | 0.0222 | Helium |  | Propylene |  |
| 212 | 0.0269 | 32 | 0.0186 | 62 | 0.0083 |
| 392 | 0.0322 | 68 | 0.0194 | 122 | 0.0093 |
| Benzen |  | Hydrogen |  | Sulfur Dioxide |  |
| 0 | 0.0065 | -172 | 0.0057 | 32 | 0.0116 |
| 40 | 0.0070 | -143.5 | 0.0062 | 64.4 | 0.0124 |
| 70 | 0.0075 | -25 | 0.0077 | 68.9 | 0.0125 |
| 100 | 0.0080 | 32 | 0.0084 | 213 | 0.0161 |
| 200 | 0.0091 | 69 | 0.0088 |  |  |
| Butene |  | 264 | 0.0108 |  |  |
| 0 | 0.0075 | Hydrogen Chloride |  |  |  |
| 40 | 0.0080 | 54.4 | 0.0139 |  |  |
| 70 | 0.0085 | 61.8 | 0.0141 |  |  |
| 100 | 0.0090 | 212 | 0.0182 |  |  |
| 200 | 0.0104 | Hydrogen Sulfide |  |  |  |
| Butylen |  | 32 | 0.0117 |  |  |
| 66 | 0.0074 | 62.6 | 0.0124 |  |  |
| 212 | 0.0095 | 212 | 0.0159 |  |  |
| Carbon Dioxide |  | Methane |  |  |  |
| -144 | 0.0090 | 32 | 0.0102 |  |  |
| -76 | 0.0106 | 68 | 0.0109 |  |  |
| 32 | 0.0139 | 212 | 0.0133 |  |  |
| 68 | 0.0148 |  |  |  |  |
| 86 | 0.0153 |  |  |  |  |




Reference


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